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3	Characterization of PAHs exposure in workplace atmospheres of a sinter plant and
4	health-risk assessment for sintering workers
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6	Yuan-Chung Lin ^{1,2,3} , Wen-Jhy Lee ^{3,4} , Shui-Jen Chen ^{4,5} ,
7	Guo-Ping Chang-Chien ^{1,2} , Perng-Jy Tsai ^{4,6*}
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8 9	¹ Department of Chemical and Materials Engineering, Cheng Shiu University,
10	Kaohsiung County 833, Taiwan.
11	² Super Micro Mass Research & Technology Center, Cheng Shiu University,
12	Kaohsiung County 833, Taiwan.
13	³ Department of Environmental Engineering, National Cheng Kung University.
14	1, University Road, Tainan 70101, Taiwan
15	⁴ Sustainable Environment Research Center, National Cheng Kung University. 1,
16	University Road, Tainan 70101, Taiwan.
17	⁵ Department of Environ mental Science and Engineering, National Pingtung University of
18	Science and Technology. 1, Shieh-Fu Rd, Nei Pu, Pingtung 91201, Taiwan,
19	⁶ Department of Environmental and Occupational Health, Medical College, National Cheng
20	Kung University. 138, Sheng-Li Road, Tainan 70428, Taiwan.
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23	
24	*Correspondence author: Perng-Jy Tsai. Department of Environmental and Occupational
25	Health, Medical College, National Cheng Kung University. 138, Sheng-Li Road, Tainan
26	704, Taiwan. Tel.: +886-6-2088390; Fax: +886-6-2752484; E-mail address:
27	pjtsai@mail.ncku.edu.tw (PJ., Tsai)

28 Abstract

29 This study first measured concentrations of polycyclic aromatic hydrocarbons (PAHs) 30 in four selected workplace atmospheres, including the raw materials inlet, sintering grate, 31 rough roll shredder and control room, and the outdoor environment of a sinter plant. Then, 32 PAHs exposures and their resultant health-risks were assessed for sintering workers. We 33 found that total PAH concentrations of the three selected sintering process areas were 34 higher than that of the control room. The above results could be explained by the filtration 35 effect of the air conditioning device installed inside the control room. PAH homologue 36 distributions of the three selected sintering process areas were significantly different from 37 that of the outdoor environment suggesting that PAHs found in the sintering workplace atmospheres were mainly contributed by process fugitives. Total PAH exposure levels were 38 39 lower than the current permissible exposure limits, thus revealing that sintering workers are 40 not a high risk group for long-term effects attributable to PAHs. Moreover, the lung cancer 41 risks associated with the above PAH exposures were lower than the significant risk level 42 defined by US Supreme Court further confirming that their exposures could be acceptable 43 at this stage.

44 **Keywords**: Polycyclic aromatic hydrocarbons, Sinter plant, Process fugitives, Exposure

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assessment, Health risk assessment

46 **1. Introduction**

47 It is known that several polycyclic aromatic hydrocarbons (PAHs) are mutagenic 48 and/or carcinogenic in rodents, and some of them are human potential carcinogens [1]. 49 PAHs can be generated from many human activities, such as industrial production, transportation, and waste incineration. In principle, the mechanisms associated with the 50 51 generation and/or depletion of PAHs in the high-temperature combustion process followed 52 three major pathways, including pyrosynthesis [2], direct emission of unburned fuel [3], 53 and thermal destruction of fuel components [4]. For iron and steel industries, PAHs are 54 released from coke manufacturing, sintering, iron making, casting, molding, cooling, and 55 steel making processes [5]. PAHs emitted from iron and steel industries has been 56 recognized as the second major source in Norway (accounting for 12% of the yearly total 57 PAH emission) [6]. Intensive studies have been conducted to investigate PAH emissions 58 from the stacks of various manufacturing processes in iron and steel industries [7]. 59 However, measurements of process fugitive PAH concentrations in workplace atmospheres 60 have been focused mainly on coke ovens [8–11]. To the best of our knowledge, PAHs concentrations in sinter plant workplaces and their resultant health-risk impact on sintering 61 62 workers have never been reported.

63 To assess health risks associated with PAH exposures, it is important to know the total 64 carcinogenic potency arising from the exposures of various PAH compounds. In principle, 65 the carcinogenic potency of a given PAH compound can be assessed according to its 66 benzo[a]pyrene equivalent concentration (BaP_{eq}). Calculating the BaP_{eq} concentration for a 67 given PAH compound requires the use of its toxic equivalent factor (TEF; using 68 benzo[a]pyrene as a reference compound) to adjust its original concentration [12-14]. 69 Among the available TEFs lists, the one established by Nisbet and LaGoy in 1992 has been 70 demonstrated to best reflect the actual state of knowledge of the toxic potency of each

individual PAH species [14]. By using the TEF list the carcinogenic potency of total PAHs
(total BaP_{eq}) can be determined as the sum of BaP_{eq} concentrations of the 21 selected PAH
compounds.

74 For estimating the lung cancer risk associated with inhalatory PAH exposures, the World Health Organization (WHO) has suggested a unit risk of 8.7×10^{-2} (µg m⁻³)⁻¹ for the 75 76 lifetime (=70 years) PAH exposure, assuming one was exposed to BaP concentration of 1 μ g m⁻³ [15]. It is worth noting that the above unit risk was proposed for lifetime exposure, 77 78 therefore, it has been adopted for assessing the exposure of general adults to the ambient 79 atmospheric PAHs [16]. For occupational exposure, Pott established a relationship between 80 BaP exposure and lung cancer risk [17], based on a data bank provided by an 81 epidemiological study conducted by Redmond et al. [18]. He suggested the unit risk of 7.0 $\times 10^{-2}$ (µg m⁻³)⁻¹ for a 25-year occupational PAHs exposure with the averaged BaP 82 concentration of 1 µg m⁻³. By using the same data bank, the US Environmental Protection 83 Administration [19], however, suggested a different unit risk of $6.4 \times 10^{-4} (\mu g m^{-3})^{-1}$ for 84 PAHs exposure based on its total PAH content (expressed as the benzene soluble fractions). 85 86 Since a recent study has indicated BaP could be a better indicator than total PAH content 87 on characterizing the carcinogenic potency of PAHs [20], the unit risk suggested by Pott in 88 1985 has been used in our previous study [21]. 89 In this study, static air samplings were conducted in the above mentioned four 90 workplaces to characterize PAH fugitive emissions from the sintering process. 91 Time/activity patterns for workers of different job titles were recorded according to our 92 field observation. By combining the above two types of information workers' PAH 93 exposure levels were assessed and their resultant health risks were estimated. 94 2. Materials and Methods

95 2.1. The selected sintering process

96 One sinter plant located in southern Taiwan, with a selective catalytic reduction (SCR) 97 air pollution control device, was selected in this study. For the selected sintering process, it first involves the mixing of iron ore fines, iron-bearing recovery materials (such as 98 99 iron-bearing dusts and slag), and fluxes (lime or dolomite) with a ~ 5 % finely divided fuel, 100 such as coke breeze or anthracite. The mixture is then placed on a traveling grate to form a 101 sintering bed. The traveling grate resembles an endless loop of a conveyor belt, forming a 102 shallow trough with small holes in the bottom. The bed is ignited by passing under an 103 ignition burner which is fired with natural gas and air. During the ignition process, the air is 104 pulled down through the bed as the grate moves slowly toward the discharge end. As the 105 coke fines burn in the bed, the generated heat sinters/or fuses the fine particles. The 106 temperature of the bed is around 1,300 to 1,500 °C. Mean production rates are 20 to 40 metric tons m⁻² d⁻¹ depending upon the characteristics of the ore materials and the sintering 107 108 conditions [22]. Typical operation conditions for the sintering process have been described 109 in more details elsewhere [23-24]. For sinter plant workers, they are required to perform 110 their work tasks at the nearby of the raw materials inlet, sintering grate, rough roll shredder, 111 and control room.

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113 2.2. Sampling strategy and worker's time/activity pattern

Three sampling sites located approximately 2 m away from the raw materials inlet (Site #1), sintering grate (Site #2), and rough roll shredder (Site #3) were selected to characterize PAH concentrations in the sintering workplaces of the selected sinter plant. For the selected sinter plant, the air introduced to the control room (located at the end of the sintering grate) was directly drawn from the workplace atmosphere of the sinter plant but was filtered by an air conditioner. Static air samplings were also conducted in the control room (Site #4) in order to characterize fugitives transferring from the sintering zone to the control room. The 121 location of the above sampling sites in the selected sintering plant are shown in Figure 1. 122 Field samplingswere also conducted on the outdoor environment located at the upwind side of the selected sinter plant (Site #5) for comparisons. All air samples were colleted by using 123 124 a high-volume PS-1 sampler (Greaseby Anderson, GA). This sampler was equipped with a quartz-fibre filter to collect PAHs of the particle phase, and followed by a XAD-16 125 126 cartridge for collecting PAHs of the gas phase. To avoid effluent stream from PS-1 dilute 127 the total suspended particle (TSP) and PAH concentration in control room, the effluent gas 128 from PS-1 sampler was discharged to the outside of the control room. The sampling flow rate was specified at ~0.18 m³ min⁻¹. Each sample was collected continuously for ~24 hrs 129 130 (i.e., sampling volume = $\sim 250 \text{ m}^3$). 131 The time/activity patterns of the four selected groups sintering workers were recorded 132 based on our field observation (Table 1). Group A (i.e., raw material charging workers) on 133 average stayed at Site #1 (raw materials inlet) and Site #4 (control room) for 1.67 hr and 134 6.33 hr, accounting for 20.8% and 79.2% of their total work time (8hr), respectively. 135 Group B (i.e., sintering grate workers) on average stayed at Site #2 (sintering grate) and 136 Site #4 for 2.5 hr and 5.5 hr, accounting for 31.2% and 68.8% of their total work time, 137 respectively. Group C (i.e., shredding workers) on average stayed in Site #3 (rough roll 138 shredder) and Site #4 for 3.0 hr and 5.0 hr, accounting for 37.5% and 62.5% of their total 139 work time, respectively. Group D (i.e., sintering process engineers and supervisors) on 140 average stayed in Site #1, Site #2, Site #3 and Site #4 for 1.33, 1.33, 1.33 and 4.0 hr, 141 accounting for 16.7%, 16.7%, 16.7% and 50.0% of their total work time, respectively. 142 143 2.3. PAH analysis 144 For PAH analysis, each collected sample (including particulate and gaseous PAH

samples) was extracted in a Soxhlet extractor with a mixed solvent (n-hexane and

146	dichloromethane; vol/vol, 1:1; 500 mL each) for 24 hrs. The extract was then concentrated
147	by nitrogen (N ₂), cleaned up by sodium sulfate and re-concentrated to exactly 1.0 mL by N ₂ .
148	PAH contents were determined using a Hewlett-Packard (HP) gas chromatograph (GC) (HP
149	6890N; Hewlett-Packard, Wilmington, DE, USA) with a mass selective detector (MSD)
150	(HP 5973) and a computer workstation (Aspire C500; Acer, Taipei, Taiwan). This GC/MSD
151	was equipped with a capillary column (HP Ultra 2, 50 m x 0.32 mm x 0.17 $\mu m)$ and an auto
152	sampler (HP-7683). It was operated under the following conditions; injection volume of 1
153	μ L, splitless injection at 310°C, an ion source temperature of 310°C, an oven from 50
154	to100°C at 20°C min ⁻¹ ; from 100 to 290°C at 3°C min ⁻¹ ; and held at 290°C for 40 min. The
155	masses of primary and secondary ions of PAHs were determined in scan mode using pure
156	PAH standards. PAHs were qualified in the selected ion monitoring (SIM) mode [25-29].
157	The PAH homologues grouped by the number of rings are naphthalene (Nap) for
158	2-ring, acenaphthylene (AcPy), acenaphthene (Acp), fluorine (Flu), phenanthrene (PA), and
159	anthracene (Ant) for 3-ring, fluoranthene (FL), pyrene (Pyr), benzo[a]anthracene (BaA),
160	and chrysene (CHR) for 4-ring, cyclopenta[c,d]pyrene (CYC), benzo[b]fluoranthene (BbF),
161	benzo[k]fluoranthene (BkF), benzo[e]pyrene (BeP), benzo(a)pyrene (BaP), perylene (PER),
162	dibenzo[a,h]anthracene (DBA), benzo[b]chrycene (BbC) for 5-ring,
163	indeno[1,2,3,-cd]pyrene (IND), benzo[ghi]perylene (Bghip) for 6-ring, and coronene (COR)
164	for 7-ring. The GC/MSD was calibrated with a diluted standard solution of 16 PAH
165	compounds (PAH mixture-610M; Supelco, Bellefonte, PA, USA) plus five additional
166	individual PAHs obtained from Merck (Darmstadt, Germany). Ten consecutive injections
167	of a PAH 610-M standard yielded an average relative standard deviation of the integrated
168	GC/MSD area of 8.02 % (range = 5.45 % to 10.33 %).
169	In this study, two internal standards (phenanthrene-d10 and perylene-d12) were used

170 to check their response factors, the recovery efficiencies for PAHs analysis and to

171 determine final concentrations. The recovery efficiencies of 21 individual PAHs and these 172 two internal standards were determined by processing a solution containing known PAH 173 concentrations through the same experimental procedure used for the samples. Recovery 174 efficiency was measured via analyzed mass of PAH divided by input mass of known PAH. 175 This study showed the recovery efficiencies for the 21 PAH compounds range from 0.795 176 to 0.972, with an average value of 0.881. The recovery efficiencies of two internal 177 standards (phenanthrene-d10 and perylene-d12) were between 85.7% and 93.5 and were 178 fairly constant. The recovery efficiencies of these two internal standards (phenanthrene-d10 179 and perylene-d12) were averaged and used for the quantification. This action will control 180 the analysis error to be less than 15%, which guarantees the reported data of this study 181 being at an excellent level. Analyses of field blanks, including aluminum foil, glass fiber 182 filter and an PUF/XAD-16 cartridge, revealed no significant contamination (GC/MSD 183 integrated area < detection limit).

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185 2.4. Data analysis

In this study, the total-PAH concentration represents the sum of the concentrations of
21 PAH compounds for each collected sample. PAHs were grouped into three categories
based on their molecular weights, including low molecular weight PAHs (LMW-PAHs,
containing two- and three-ringed PAHs), middle molecular weight PAHs (MMW-PAHs,
containing four-ringed PAHs), and high molecular weight PAHs (HMW-PAHs, containing
five- to seven-ringed PAHs).

In this study, the carcinogenic potencies associated with PAH emissions to each
workplace atmosphere were also determined. Here, the carcinogenic potency of a given
PAH compound was assessed according to its benzo[a]pyrene equivalent concentration (i.e.,
BaP_{eq}) by using the TEFs list established by Nisbet and LaGoy in 1992 [14]. The

196	carcinogenic potency of total PAHs (i.e., total BaP _{eq}) was determined as the sum of BaP _{eq}
197	concentrations of the 21 selected PAH compounds. To assess workers' excessive lung
198	cancer risks associated with a 25-yr occupational exposure, the unit risk suggested by Pott
199	in 1985 (= 7×10^{-5} (BaPeq ng m ⁻³) ⁻¹) was used in the present study [17]. This is mainly
200	because BaP is a better indicator than total PAH content on characterizing the carcinogenic
201	potency of PAHs [20].

All measured and estimated concentrations were presented in their means \pm standard deviation (\pm SD). Statistical significance was examined by using the *t*-test.

204 **3. Results and Discussion**

205 3.1. TSP concentrations in sintering workplaces and the outdoor environment

Table 2 shows the mean total suspended particle (TSP) concentrations of the four selected workplaces and the outdoor environment of the selected sinter plant. For the four selected workplaces, the highest TSP was found at Site #1 (=2690 μ g Nm⁻³), which was considered due to dust emissions from the raw material charging process. The second and third highest TSP were found at Site #2 and Site #3 (=2130 and 1600 μ g Nm⁻³,

211 respectively), but their concentrations were much lower than that of Site #1 (p < 0.05). This

212 might be because the strong airflow was pulled down through the sintering bed resulting in

213 less fugitive TSP emitted into the sintering zone. TSP concentrations in Site #1, Site #2 and

Site #3 were 18.4, 14.6 and 10.9 times in magnitude higher than that in Site #4 (=146 μ g

215 Nm⁻³) (p < 0.05). This might be explained either by the location of the control room being

216 far away from the sintering process, or by the filtration efficiency (TSP reduction fraction

217 >95%) of the air conditioning device used in the control room. The permissible TSP

218 concentration in workplace environment in Taiwan is 10,000 µg Nm⁻³, which was

significantly higher than that of Site #1–Site #4 (p<0.05). Nevertheless, it should be noted

that the concentrations found in Site #1–Site #3 were still higher than that of the outdoor

environment (i.e., Site $\#5 = 143 \ \mu g \ Nm^{-3}$) (*p*<0.05). The above result suggests that TSP concentrations found in the sintering process areas were mainly contributed by the process fugitives, rather than those transported from the outdoor environment.

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3.2. Characterization of PAH concentrations in sintering workplaces and the outdoor environment

Table 3 shows the mean PAH concentrations (gas- + particle-phase) of the four 227 228 selected workplaces and the outdoor environment of the sinter plant. For the mean total PAH concentrations, we found that Site #2 (30.4 µg Nm⁻³) was significantly higher than 229 that of Site #1 (17.9 μ g Nm⁻³) and Site #3 (16.3 μ g Nm⁻³) (p<0.05), which was considered 230 231 due to molten process in the furnace. The concentrations found in the above three selected sintering zone workplaces were significantly higher than that of the Site #4 (8.37 μ g Nm⁻³) 232 233 (p < 0.05). The relatively low total PAH concentrations found in the Site #4 (i.e., control 234 room) could be explained again either by its location being far away from the sintering 235 zone, or the filtration effect of the air conditioning device used in the control room. 236 Moreover, we also found that the PAH concentrations obtained from the sintering zones (Site #1-Site $\#3 = 16.3 - 30.4 \mu g \text{ Nm}^{-3}$) were much higher than that of outdoor environment 237 (Site $\#5 = 7.42 \mu \text{g Nm}^{-3}$) (p<0.05). The above results further confirmed that PAHs found in 238 239 the workplace atmospheres could be mainly contributed by sintering process fugitives. 240 rather than that transported from the outdoor environment. 241 Regarding the measured total BaP_{eq} concentrations (i.e., gas- + particle-phase), the

concentration found in the Site #2 (0.16 μ g Nm⁻³) was higher than those found in Site #1 and Site #3 (0.12 and 0.13 μ g Nm⁻³, respectively) (*p*<0.05). The pattern was similar to that found in the corresponding total PAH concentrations, since the above three selected sampling sites shared with similar PAH homologue distributions. Finally, total BaP_{eq}

246	concentrations found in sintering zone workplaces (i.e., Site #1, Site #2, and Site #3) were
247	much higher than that of the Site #4 (0.040 μ g Nm ⁻³) (p <0.05). The above results suggest
248	that the isolation of the control room and the ventilation measures had a useful impact on
249	PAHs exposure profile, especially by lowering the concentrations of carcinogenic species.
250	Table 3 also shows the PAH homologue distributions of the 5 selected sampling sites.
251	We found the fractions of LMW-, MMW-, and HMW-PAHs in total-PAHs were quite
252	similar among Site #1 (86.5%, 9.52%, and 4.01%, respectively), Site #2 (86.7%, 9.60%,
253	and 3.71%, respectively), and Site #3 (86.3%, 8.53%, and 5.16%, respectively). The above
254	results again suggests PAHs found in the sintering zone were of the same nature (i.e.,
255	emitted from the sintering process with a similar coagulation effect due to their low
256	concentrations). On the other hand, a very different pattern was found in Site #4 (91.4%,
257	6.09%, and 2.51%, respectively). Less fractions in both MMW- and HMW-PAHs found in
258	Site #4 could be because less particle-phase PAHs were found in the control room,
259	considering both MMW- and HMW-PAHs were mainly presented in particle-phase due to
260	their low volatile characteristics. Finally, a very different pattern was found in the outdoor
261	environment (79.5%, 16.4%, and 4.18%, respectively) further confirmed our previous
262	inference: PAHs found in the workplace atmospheres were mainly contributed by process
263	fugitives, rather than those transported from the outdoor environment.
264	3.3 Gas- and particle-phase PAHs containing in total PAH and total BaP _{ea}

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concentrations in the workplace atmospheres

266 Table 4 shows gas- and particle-phase PAHs containing in total PAH and total BaP_{eq}

267 concentrations for samples collected from the workplace atmosphere of the selected sinter

- 268 plant. For total PAH, concentrations of the gas-phase PAHs (8.33-30.1 µg Nm⁻³, accounting
- 269 for 98.3%-99.5% total PAHs) were consistently higher than that of particle-phase
- 270 $(0.042-0.365 \ \mu g \ Nm^{-3})$, accounting for 0.5%-1.7% total PAHs) for any given studied

271 workplaces (p < 0.05). The above results can be explained by total PAHs were dominated by

272 LMW-PAHs (Table 3). For total BaP_{eq}, concentrations of the gas-phase (0.037-0.121 μg

273 Nm⁻³) were also higher than that of particle-phase (0.003-0.039 μ g Nm⁻³) for any given

studied workplaces (p < 0.05). However, particle-phase PAHs had more contribution to total

BaP_{eq} (8.1-24.1%) than to total PAHs (0.5%-1.7%). The above results can be explained by

total PAHs were dominated by LMW-PAHs which are known with low TEFs (Table 3).

Finally, it should be noted that the concentrations of both gas- and particle-phase

278 PAHs found in the outdoor environment (site #5) were consistently lower than that of the

sintering zone (i.e., Site #1-Site #3) (p < 0.05) (Table 4). Particularly, the contributions of

280 gas- and particle-phase PAHs to both total PAHs and total BaP_{eq} for samples collected from

the outdoor environment were quite different from that of sintering zone (p < 0.05) (Table 4).

282 The above results further confirm that PAHs found in the workplace environments were

283 mainly contributed by the process fugitives rather than the outdoor environment.

284 3.4. Health-risk assessment for sintering workers exposed to PAHs

In this study, worker's time-weighted average exposure was estimated based on thefollowing equation:

287 $C_{ave} = (C_i \times T_i) / \Sigma T_i$

288 Where, Cave was the worker's time-weighted average exposure to total PAHs (denoted as

total PAHs_{ave}) and total BaPeq (denoted as total BaPeq_{ave}); C_i was the worker's exposure

290 concentration to total PAHs at the i^{th} site (i.e., total PAHs_i, see Table 3) and to total BaPeq

at the i^{th} site (i.e., total BaPeq_i, see Table 2); T_i was the time of the given worker spent at

292 the ith site (see Table 1); and ΣT_i was the time for the given worker spent at all involved

work sites.

Table 5 shows total PAHs_{ave} and total BaPeq_{ave}, and their corresponding gas-phase and particle-phase concentrations. In addition, the estimated lung cancer risks for the four

selected exposure groups based on their total BaPeqave and the corresponding gas-phase and 296 297 particle-phase concentrations were also presented in Table 5. For total PAHs_{ave}, its corresponding gas-phase concentration (=82.3-121 ng m⁻³) was consistently higher than 298 that of particle phase (=0.685-23.3 ng m⁻³) (p < 0.05). Particularly, all selected exposure 299 groups were found with total PAHs_{ave} (=83.0-122 ng m⁻³) significantly lower than the 300 current permissible exposure limit regulated in Taiwan for PAHs (= $200,000 \text{ ng/m}^3$) 301 (p < 0.05). The above results suggest that PAH exposures to sintering workers might not be 302 particularly significant. In this study, the unit risk suggested by Pott in 1985 ($=7 \times 10^{-5}$ 303 (BaPeq ng m⁻³)⁻¹) was used to assess workers' any excess of risk for lung cancer associated 304 with a 25-yr occupational exposure [17]. We found that the total BaP_{ave} fell to the range of 305 0.454-0.705 ng m⁻³. The corresponding gas-phase concentration (=0.450-0.614 ng m⁻³) 306 was significantly higher than that of particle-phase (=0.004-0.137 ng m⁻³) (p < 0.05) 307 308 suggesting that the former had a more contribution on worker's lung cancer risk. However, 309 by taking both gas- and particle-phase together (i.e., total BaPave), the resultant lung cancer risks $(=3.18 \times 10^{-5} - 4.98 \times 10^{-5})$ were consistently lower than the significant risk level $(=10^{-3})$ 310 311 which was defined by the US Supreme Court [30]. The above results further confirm that 312 PAH exposures to sintering workers might be acceptable at this stage.

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314 4. Conclusions

The present paper shows that both TSP and total PAH concentrations of the three selected sintering process areas were higher than that of the control room. The above results could be explained by the filtration efficiency of the air conditioning device installed inside the control room. PAH homologue distributions of the three selected sintering process areas were significantly different from that of the outdoor environment suggesting that PAHs found in the sintering workplace atmospheres were mainly contributed by process fugitives. 321 Total PAH exposure levels in the selected areas of the sintering plant were lower than the 322 current permissible exposure limits, thus suggesting that sintering workers are usually exposed to quite low PAH concentrations. Consistently, our risk estimate for the lung 323 324 cancer risks associated with the above PAH exposures gave lower values as compared to 325 the significant risk level defined by US Supreme Court. 326 327 Acknowledgments: This research was supported in part by the Institute of Occupational 328 Safety and Health (IOSH) of the Council of Labor Affairs in Taiwan. Mr. H.C. Hou and 329 Miss UnSam Ha, Department of Environmental Engineering, National Cheng Kung 330 University, are appreciated for assisting in the laboratory work. 331 332 References Internal Agency for Research on Cancer, IARC monographs on evaluation of 333 [1] 334 carcinogenic risks to humans, overall evaluation of carcinogenicity: An updating of 335 monographs. IARC Monogr. Eval. Carcinog. Risk Chem. Hum., Lyon, 1-42(1987) 336 1-440. http://monographs.iarc.fr A. Bjørseth, Handbook of polycyclic aromatic hydrocarbons, vol. 1. Marcel Dekker, 337 [2] 338 New York, 1983. P.T. Williams, M.K. Abbass, G.E. Andrews, Diesel particulate emission: the role of 339 [3] unburned fuel, Combustion Flame 75(1989) 1-24. 340 341 P.J. Tancell, M.M. Rhead, R.D. Pemberton, J. Braven, Survival of polycylic [4] 342 aromatic hydrocarbons during diesel combustion, Environ. Sci. Technol. 29(1995) 2871-2876. 343 [5] 344 D. Nelson, P.A. Scheff, C. Keil, Characterization of volatile organic compounds 345 contained in coke plant emissions. In: The 84th Annual meeting & Exhibition of Air

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Table Captions

420	Table 1	Time/activity patterns for the four selected groups of workers of the Group A:
421		raw material charging workers, Group B: sintering grate workers, Group C:
422		shredding workers, and Group D: sintering process engineers and supervisors
423		at the four selected workplaces inside the sinter plant of the Site #1: raw
424		materials inlet, Site #2: sintering grate, Site #3: Rough roll shredder, and Site
425		#4: control room
426	Table 2	Mean TSP concentrations (\pm SD) of the four selected workplaces inside the
427		sinter plant of the Site #1: raw materials inlet, Site #2: sintering grate, Site
428		#3: Rough roll shredder, and Site #4: control room, and its outdoor
429		environment (Site #5)
430	Table 3	Mean PAH concentrations (\pm SD) of the four selected workplace atmospheres
431		of the sinter plant of the Site #1: raw materials inlet, Site #2: sintering grate,
432		Site #3: Rough roll shredder, and Site #4: control room, and its outdoor
433		environment (Site #5)
434	Table 4	Mean PAH concentrations (\pm SD) of the four selected workplace atmospheres
435		of the sinter plant of the Site #1: raw materials inlet, Site #2: sintering grate,
436		Site #3: Rough roll shredder, and Site #4: control room, and its outdoor
437		environment (Site #5)

438	Table 5	Time-weighted average exposure levels (\pm SD) of total PAHs _{ave} and total
439		BaPeq _{ave} and their corresponding particle-phase and gas-phase exposure
440		levels (\pm SD), and the resultant lung cancer risks (\pm SD) for the four selected
441		exposure groups of the Group A: raw material charging workers, Group B:
442		sintering grate workers, Group C: shredding workers, and Group D: sintering
443		process engineers and supervisors
444		
445	Figure (Caption

446 Figure 1 Sampling sites in the selected sintering plant

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